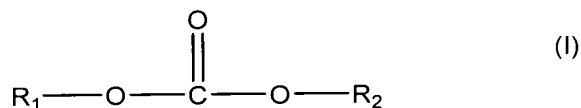


AMENDMENTS TO THE CLAIMS

Please cancel claims 33 and 35, and amend claim 21, as follows:

Claims 1-20 (Cancelled).

Claim 21 (Currently Amended) A process for recycling expanded polystyrene comprising:  
volume reduction of expanded polystyrene by dissolution in a solution comprising a dialkyl carbonate, or a blend of dialkyl carbonates, having the following general formula (I):



wherein R<sub>1</sub> and R<sub>2</sub> are the same or different and each independently represent a linear, a branched or a cyclic alkyl radical having from 1 to 12 carbon atoms, and the sum of the carbon atoms of R<sub>1</sub> and R<sub>2</sub> is from 2 to 15;

removal of an insoluble component, if present;

selective precipitation of polystyrene with a non-solvent, wherein said selective precipitation of polystyrene is carried out at a temperature of 10-70°C, wherein the non-solvent is an alkylene carbonate, or a blend of non-solvents consisting of an alcohol and an alkylene carbonate, and wherein a weight ratio of the non-solvent to the dialkyl carbonate is from 2:1 to 20:1;

separation of precipitated polystyrene; and

drying of precipitated polystyrene.

Claim 22 (Previously Presented) The process according to claim 21, wherein R<sub>1</sub> and R<sub>2</sub> each independently represent a linear or a branched alkyl radical having from 1 to 8 carbon atoms, and the sum of the carbon atoms of R<sub>1</sub> and R<sub>2</sub> is from 5 to 10.

Claim 23 (Previously Presented) The process according to claim 22, wherein the dialkyl carbonate, or blend thereof, is selected from dialkyl carbonates having a flash point higher than 55°C.

Claim 24 (Previously Presented) The process according to claim 21, wherein the dialkyl carbonate, or blend thereof, is selected from dialkyl carbonates having a flash point higher than 55°C.

Claim 25 (Previously Presented) The process according to claim 21, wherein the dialkyl carbonates are selected from the group consisting of di-n-butyl carbonate, di-iso-butyl carbonate and di-n-propyl carbonate.

Claim 26 (Previously Presented) The process according to claim 21, wherein said dissolution is carried out under atmospheric pressure at a temperature of 20-70°C with optional stirring, and the concentration of expanded polystyrene in the solution is 5-50 wt. %.

Claim 27 (Previously Presented) The process according to claim 21, wherein said dissolution is carried out under atmospheric pressure at room temperature with stirring, and the concentration of expanded polystyrene in the solution is 15-40 wt. %.

Claim 28 (Previously Presented) The process according to claim 21, wherein the insoluble component is present and said removal thereof from the solution is carried out by decanting, filtration or centrifugation.

Claim 29 (Previously Presented) The process according to claim 21, wherein said selective precipitation of polystyrene is carried out by feeding the solution to the non-solvent under stirring.

Claim 30 (Previously Presented) The process according to claim 29, wherein said selective precipitation of polystyrene is carried out by feeding the solution into a bottom portion of a precipitation reactor below a stirring system.

Claim 31 (Previously Presented) The process according to claim 29, wherein said selective precipitation of polystyrene is carried out by feeding the solution to the non-solvent at a flow rate of 30-1,500 g of solution per hour per liter of non-solvent.

Claim 32 (Previously Presented) The process according to claim 29, wherein said selective precipitation of polystyrene is carried out by feeding the solution to the non-solvent at a flow rate of 50-800 g of solution per hour per liter of non-solvent.

Claim 33 (Cancelled).

Claim 34 (Previously Presented) The process according to claim 21, wherein said selective precipitation of polystyrene is carried out at a temperature of 15-60°C.

Claim 35 (Cancelled).

Claim 36 (Previously Presented) The process according to claim 21, wherein said selective precipitation of polystyrene is carried out with a weight ratio of the non-solvent to the dialkyl carbonate of 3-15:1.

Claim 37 (Previously Presented) The process according to claim 21, wherein the non-solvent is an alkylene carbonate selected from the group consisting of propylene carbonate, ethylene carbonate and butylene carbonate.

Claim 38 (Previously Presented) The process according to claim 21, wherein the non-solvent is a blend of non-solvents consisting of an alcohol and an alkylene carbonate, wherein the alcohol is one or more alcohols selected from the group consisting of n-butyl alcohol and iso-propyl alcohol, and the alkylene carbonate is one or more alkylene carbonates selected from the group consisting of propylene carbonate, ethylene carbonate and butylene carbonate.

Claim 39 (Previously Presented) The process according to claim 21, wherein said separation of precipitated polystyrene is carried out by decanting, filtration or centrifugation, at a temperature of 10-70°C.

Claim 40 (Previously Presented) The process according to claim 21, wherein said separation of precipitated polystyrene is carried out by decanting, filtration or centrifugation, at a temperature of 15-60°C.

Claim 41 (Previously Presented) The process according to claim 21, wherein said process further comprises, after said separation and before said drying of precipitated polystyrene, washing of precipitated polystyrene at a temperature of 10-80°C with a method selected from the group consisting of:

pouring the non-solvent onto a filter comprising precipitated polystyrene;  
suspending precipitated polystyrene in the non-solvent under stirring; and  
continuous extraction of precipitated polystyrene with the non-solvent.

Claim 42 (Previously Presented) The process according to claim 21, wherein said drying of precipitated polystyrene is carried out at a temperature of 50-180°C under a pressure of 1-760 mm Hg.

Claim 43 (Previously Presented) The process according to claim 21, wherein said drying of precipitated polystyrene is carried out at a temperature of 80-150°C under a pressure of 10-500 mm Hg.

Claim 44 (Previously Presented) The process according to claim 21, wherein said process further comprises, after said drying of precipitated polystyrene, extrusion of precipitated polystyrene.